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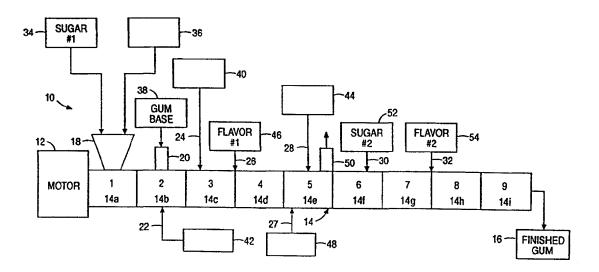
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(54) Title: METHOD FOR CONTINUOUSLY PRODUCING CHEWING GUM



(57) Abstract

An improved process for continuously producing chewing gum products. A continuous extrusion machine is utilized preferably with a rotating twin-screw mixing mechanism (10). The sugar ingredient of the chewing gum product is divided into two portions to improve texture of the final product. One portion (34) is added at the initial upstream end of the extrusion process, while the other portion (52) is added after most of the other ingredients have been included in the gum mass. The flavoring ingredients can also be divided into two portions, one portion (46) introduced into the extrusion process upstream of the sugar material and the other portion (54) introduced downstream of the other ingredients. Splitting the sugar and flavoring ingredients affects the texture and flavor release profiles of the final gum product (16).

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METHOD FOR CONTINUOUSLY PRODUCING CHEWING GUM

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Technical Field

This invention relates to improved processes for continuously producing gums, such as chewing gums and bubble gums, which have improved texture and flavor release.

Background Of The Invention

There are several systems known today for producing gum bases and final gum products, such as chewing gums and bubble gums. The present invention can be used with all types of sugared chewing gums and bubble gums. For ease of reference, all such gums will be referred to herein by the single term "chewing gum". Typically, the chewing gum base is made separately from the final chewing gum product, although there are several systems which are capable of producing a final chewing gum product in one continuous process.

In general, a chewing gum composition typically comprises a water-soluble bulk portion, a water-insoluble chewing gum base portion, and typically water and soluble flavoring agents. The insoluble gum base generally comprises elastomers, elastomer solvents, fillers, resins, polyvinyl acetate (PVA), fats, plasticizers, waxes, emulsifiers, and other miscellaneous ingredients. The flavoring can be added in various forms, and can either be sugar based for sweetness or acid based for sourness or tartness. The water-soluble portion of the gum composition decimates with a portion of the flavoring agents over a period of time during chewing. The gum base

portion is retained in the mouth throughout the time the product is chewed.

Numerous chewing gums and chewing gum bases in the past have been produced using a batch method. Single blade batch mixers are typically used for these processes. The gum base ingredients are added either separately or simultaneously into the batch mixer and the materials are melted and mixed over time. After the gum base is processed, the molten gum base batch is emptied into coated or lined pans, or transferred to other equipment such as holding tanks or filling devices, then extruded or cast into shape, and allowed to cool and solidify, before being ready for use in a chewing gum.

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When the final chewing gum products are processed using a batch method, portions of the gum base, together with softeners and bulking agents, are added to the mixer. Later, flavorings such as flavored oils and/or spray-dried flavors (sweeteners or acids) are added while mixing is continued until a homogenous mass is achieved. Systems of this type is shown, for example, in U.S. Patent Nos. 4,816,265, 5,000,965 and 5,057,328. The chewing gum mass is then cooled and later rolled, scored, and wrapped into the final product.

Continuous extrusion machines have also been used for producing chewing gum bases and the final chewing gum products, or both. The use of continuous extruders to make a final chewing gum product is shown, for example, is U.S. Patent No. 5,135,762 to Degady et al., U.S. Patent No. 5,045,325 to Lesko et al., and U.S. Patent No. 4,555,407 to Kramer et al. Processes known in the art for continuously producing a chewing gum base with the use of a continuous extrusion machine are shown, for example, in U.S. Patent Nos. 5,419,919 and 5,486,366 both to Song et al.

The chewing gum base and chewing gum product processes disclosed in these patents typically utilize a continuous extrusion machine, such as a twin-screw extruder. These extruders typically have several different feed inlets were the ingredients are added. The elongated screws inside the barrels of the extruders are equipped with different types of elements. Continuous extrusion machines that can be used for producing chewing gum bases and final chewing gum products include extruders from Togum, Baker Perkins, Werner & Pfleiderer Steel Works, Leistriztz, Corp., Japan WLS, and Buss Manufacturing Company.

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several efforts have been attempted in the past to extend the flavor of chewing gums over a longer period of time. These efforts include, for example, a controlled release of flavoring, micro-encapsulation of flavoring or other materials, and the like. Such systems are shown, for example, in U.S. Patent Nos. 5,057,328 to Cherukuri et al. and 5,116,627 to Rutherford et al. Other methods involve granulating or agglomerating ingredients into a granular matrix to provide for a more controlled release of ingredients. This is shown, for example, in U.S. Patent No. 5,124,160 to Zibell et al. Efforts have also been made to change the texture of the final chewing gum product.

It is a general object of the present invention to provide an improved process for the production of chewing gum products. It is also an object of the present invention to provide an improved process for increasing the length of the flavor profile for the chewing gum product.

It is still another object of the present invention

to provide a system for continuously preparing chewing gum

products which have a controlled texture profile as well as a

controlled flavor profile. It is a further object of the

present invention to provide an improved process for continuously producing chewing gum products in which the flavor is released more slowly and evenly than in known chewing gum products.

These and other objects are met by the present invention in which a preferred form of the invention is described hereinafter.

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Summary Of The Invention

The present invention provides an improved system for continuously producing a chewing gum product. In particular, the present invention provides an improved process for producing a final chewing gum product which has an improved texture and which can have its flavor profile changed as desired to have an initial "burst" of flavor and/or a slower and longer release of flavor.

In accordance with the present invention, continuous extrusion processor is used to produce the chewing Various ingredients are added to the extruder, including a gum base, sugar, softeners, plasticizers, oils and The sugar is divided into two portions with one portion being added at the beginning of the extrusion process and the other portion being added as one of the last ingredients. Dividing the sugar into two portions affects the texture of the final chewing gum product and makes it smoother and more chewable. Adding the flavor downstream of the other ingredients creates an initial "burst" of flavor when the gum Splitting the flavor and adding a portion of it is chewed. upstream changes the flavor profile of the gum and creates a slower and more even release of the flavor throughout the chew.

Any conventional flavorings can be used with the present invention, including sweet flavorings and sour or tart flavorings.

Dividing the sugar material in the extruder, together with controlling other extrusion parameters, such as the speed of the extruder and the temperatures of the various extrusion barrels, allows control of the flavor and texture profiles and allows production of various types of chewing gum products.

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The present invention allows a better quality final product to be prepared, as well as a product in which the flavor can be released in different amounts and at different times in the chew.

These and other features, advantages, and benefits of the present invention will become apparent from a review of the following description, when taken in view of the accompanying drawings and appended claims.

Brief Description Of The Drawings

FIGURE 1 is a schematic diagram of a continuous

20 chewing gum system in accordance with the present invention; and

FIGURE 2 depicts the system of Figure 1 in which a
side feeder is utilized.

Best Modes For Carrying Out The Invention

Referring to Figure 1, a continuous chewing gum
manufacturing process is shown schematically which utilizes an
extrusion mixer 10. The extruder 10 can be of any conventional
type and has a motor and control mechanism 12 and an elongated
barrel member 14. The continuous extruder 10 can be of any
conventional type available from many extruder manufacturers
known today, such as Japan Steel Works, Leistriztz, Werner &

Pfleiderer Corp., Togum, WLS, Baker Perkins, and/or Buss Manufacturing Company. Preferably, however, the continuous extruder 10 is a co-rotating twin screw extruder.

Typically, the continuous extrusion machines use twin-screw mechanisms which are either co-rotational, counter-rotational, intermeshing or tangential. These extruders have one or two elongated screw members in the barrels 14 which intermix and process ingredients and materials for the final gum product 16. The elongated screw members have different types of screw elements on them for processing the materials that are fed into the barrel 14.

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The elongated screw members utilize different types of screw elements for processing the materials in the extruder. The most common types of screw elements include conveying elements, compression elements, reverse conveyance elements, homogenizing elements such as shearing disks and tooth elements, and kneading disks and kneading blocks. These elements, and other elements typically used in extruding machines, especially twin-screw extruders, are well known in the art and are commercially available. The elements are often specifically designed for the particular type of extruder utilized and the particular type of ingredients utilized in the final desired product.

The extruders typically have a number of separate stages along the length of the barrel 14. In the preferred Werner & Pfleiderer embodiment shown in Figure 1, nine separate barrel sections or members are provided (numbered 1-9). Each of the barrel sections 14a through 14i are separately heated and cooled in order to maintain the material within the barrel at an appropriate processing temperature and consistency.

The extruders typically have several different feed inlets where the ingredients are added. For example, as shown

in Figure 1, the extruder 10 has a first feed inlet 18 as well as other inlets 20, 22, 24, 26, 27, 28, 30 and 32 positioned downstream on the barrel 14. Typically solid ingredients, such as sugar 34 and salvage 36 are introduced into the barrel through the upstream initial inlet port 18. Other ingredients, usually in a liquid condition, are introduced into one or more of the downstream ports. These other ingredients include, for example, gum base 38, softeners or plasticizers, such as corn syrup 40, lecithin 42 and oil 44, flavorings 46, and coloring 48.

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The chewing gum ingredients are added to the barrel of the extruder through one or more conventional mechanisms or systems. For example, the sugar 34 and salvage materials 36 can be added by conventional loss-in-weight (LTW) feeders. The LTW feeders meter and regulate the flow of material into the barrel 14. The gum base 38 is typically introduced into the extruder in a molten condition by means of a conventional metering and pumping system. The softeners, plasticizers, oils and coloring are liquid materials and are typically added into the barrel through conventional liquid metering and pumping systems. The flavoring materials or ingredients 46 are typically injected into the barrel 14 by means of a conventional liquid injection system.

The second portion 52 (sugar #2) of the sugar ingredient can also be added to the main extruder 10' by the use of a conventional side feeder apparatus 60, as shown in Figure 2.

In the barrel 14, the material and ingredients are introduced into the screw cavity in barrel sections or members 30 14a-14f (Nos. 1-6) where they are mixed together forming a homogeneous mass. The mixed material is then compressed in barrel sections 14g-14i (Nos. 7-9) where the internal cavity is

filled and pressure is built up. A vent 50 is typically provided between the mixing and compression sections of the barrel to eliminate undesired build up of gases prior to the mass of material entering the compression portion of the barrel.

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In order to introduce certain materials into the extrusion process, it is also possible to use a side feeder. The side feeder can be any conventional extrusion apparatus, such as those available from Buss Manufacturing Company, Baker Perkins, and Werner & Pfleiderer Corp. The side feeder has a motor and control mechanism and an elongated barrel. An inlet chute is used to supply materials to the side feeder. The side feeder is connected to the main extruder, preferably, with an adaptor mechanism.

The gum base 32 is typically intermixed with a filler of some type, such as dicalcium phosphate. The dicalcium phosphate acts as a lubricant or dusting agent, and other conventional materials could be used for that same purpose, such as talc or atomite.

Once the gum materials are introduced into the extruder 10, they are conveyed by the elongated screws along the length of the barrel 14. The final gum product 16 is extruded from the extruder 10 at the downstream end.

In accordance with the present invention, certain selected ingredients of the chewing gum product are or can be divided into two portions so that they can be added at different stages in the extrusion process in order to secure different profiles of texture and flavoring. In particular, the sugar and flavoring ingredients can be split into two portions in accordance with the present invention.

As shown in Figure 1, the sugar ingredient is added at two separate locations in the gum producing system. The sugar is divided into two portions (sugar #1-34 and sugar #2-

52), each portion having substantially the same size and volume. The first portion or quantity of sugar 34 is added at the upstream or initial end of the extrusion process, preferably at inlet chute 18 in barrel section 14a (No. 1). The second portion or quantity of sugar 52 is added at a position downstream of all of the other ingredients, such as at barrel section 14f (No. 6).

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Splitting the sugar material into two portions and adding them at separate locations in the gum extrusion process affects the graininess and texture of the final product. It results in a more uniform and less granular final gum product than if all the sugar is added at one time and in one location. (Adding all of the required sugar at location 14f (No. 6) results in a less uniform and grainier final gum product.) Adding the sugar at two separate locations also allows the sugar to be blended and mixed into the material mass more evenly, which provides a better sweetness profile over time for the final gum product when it is chewed.

Although the preferred process in accordance with the present invention divides the sugar material into two portions having substantially the same weight and amount, it is also possible to divide the sugar into two portions which differ significantly in weight and amount. For example, adding 60-75% of the sugar material at the downstream location (barrel section 14f) and adding the remaining 25-40% of the sugar material at the initial chute (barrel section 14a) is possible, although it may result in a final gum material which is not as soft as that produced by the preferred process.

The flavor ingredient can also be divided and added in two portions and positions in the extrusion process. For example, the flavor can be divided into two portions with the first portion 46 (Flavor #1) being added at port 26 and the

second portion 54 (Flavor #2) being added at the intersection port 32 between barrels 14g and 14h. By adding a portion of the flavor at an upstream portion of the extruder, the flavoring is incorporated more evenly and thoroughly into the gum material in the extruder and results in a more even and longer lasting flavor release in the final product. By adding a portion of the flavor at a downstream port, such as at 32 between barrel sections 14g and 14h, an initial "burst" of flavor can be provided in the final gum product 16.

As indicated above, the flavoring which can be used for the gum product can either be a sweet flavoring or a sour or tart flavoring, each of which is conventionally known in the chewing gum field. In this regard, sour or tart flavorings are typically provided by the addition of a citric acid.

Auxiliary systems (not shown) which aid in the addition and injection of the solid or liquid ingredients into the extruder 10 are positioned along the length of the extruder. Such feeding systems which may include pumping and conveying elements, side feeders, gravity feeders and the like, are all conventionally known and do not have to be shown in detail herein.

If an acid material is added to the extruder 10 in order to get a sour finished gum product, then the amount of acid added should be regulated relative to the amount of sugar in order to prevent graininess in the final product. The acid materials are typically added in a granular condition and if more than 2 - 3 percent of acid materials are added to the composition, then the splitting of the sugar material into two portions is necessary in order to prevent or minimize the graininess of the final finished gum product.

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Also, the speed of the extruder can be changed to control the texture and "hardness" of the final finished gum

product 16. The faster the extruder speed, the softer the final gum product since the gum base elastomer is broken down more effectively. On the other hand, the slower the speed of the extruder, then the harder the gum as less elastomer is broken down. The optimum extruder screw speed can be selected by trial-and-error for the particular extruder and gum material utilized.

It is also possible to add solid salvage into the final finished gum extrusion process by a side feeder (not shown).

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Preferably, the temperature of the extrusion process in the extruder 10 is kept to a minimum. The conveying elements should provide a minimum build-up of temperature in the barrel 14 and provide a low sheer mixing process. For this purpose, 15 each of the barrel sections 14a-14i are separately cooled with a glycol-water mixture and kept at approximately OEF. A low temperature is important since it eliminates or minimizes the volatilization of the flavoring in the material in the extruder. This is particularly preferable since flavoring ingredients are 20 often the most expensive ingredients in the gum composition. In this regard, it is preferred to run the twin-screw extrusion machine on the order of 50 - 100 revolutions per minute (RPM) and keep the temperature of the gum material in the range of 110 - 125EF.

25 While the best modes for carrying out the invention have been described in detail, those familiar with the art to which this invention relates will recognize various alternative designs and embodiments for practicing the invention within the scope of the appended claims.

What Is Claimed:

1. A method of continuously producing chewing gum materials in a continuous extrusion mixer, said gum materials including such ingredients as gum base, sugar, flavorings, softeners and plasticizers, said method comprising the steps of: dividing the sugar ingredient of the gum material

dividing the sugar ingredient of the gum material into two portions;

introducing a first portion of the sugar ingredient into a first section of the extrusion mixer;

introducing a second portion of the sugar ingredient into a second section of the extrusion mixer downstream of the first section;

wherein the texture profile of the final chewing gum material is improved.

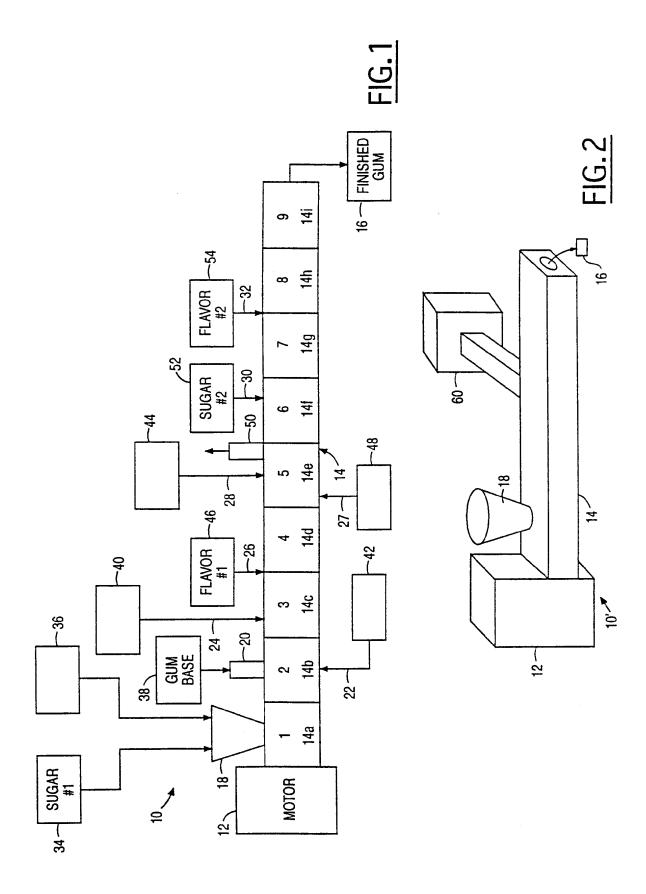
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- 2. The method as set forth in claim 1 wherein said extrusion mixer has at least three sections with said first section being the initial upstream end of said mixer, said second section being downstream of said first section, and with a third section being positioned in between said first and second sections, and wherein said method further comprises the step of introducing the gum base, flavorings, and other ingredients into said extrusion mixer in said third section.
- 3. The method as set forth in claim 2 further comprising the step of dividing the flavoring ingredient of the gum material into a first flavor portion and a second flavor portion, and introducing said first flavor portion into said third section and introducing said second flavor portion downstream of said second portion of the sugar ingredient,

wherein an initial burst of flavor is experienced when the final gum material is chewed.



INTERNATIONAL SEARCH REPORT

Inter nal Application No PCT/US 98/24680

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А	US 4 409 244 A (CHERUKURI ET AL. 11 October 1983 see column 3, line 45 - column 4 claim 5		1
A	US 5 612 071 A (SONG ET AL.) 18 see column 9, line 65 - column 3 figures 7-10		1-3
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	atent document I in search report		Publication date		atent family member(s)		Publication date
US	4555407	Α	26-11-1985	CA EP	1253735 0191986		09-05-1989 27-08-1986
	•			JP	61162136		22-07-1986
US	4409244	A	11-10-1983	NONE			
US	5612071	Α	18-03-1997	US	5543160		06-08-1996
				AU AU	1991495 1992895		29-03-1996
				AU	1992695		29-03-1996 29-03-1996
				AU	1999295	Α	29-03-1996
				AU	2117995	Α	29-03-1996
				AU	688935		19-03-1998
				AU AU	3062095 689293		28-03-1996 26-03-1998
				AU	3062195		28-03-1998 28-03-1996
				AU	689294	В	26-03-1998
				AU	3062295		28-03-1996
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				CA	2199606		21-03-1996
				CA CA	2199607		21-03-1996
				CA	2199608 2199712		21-03-1996 21-03-1996
				. CA	2232852		14-03-1996
				CN	1157555	Α	20-08-1997
				CN	1157556	Α	20-08-1997